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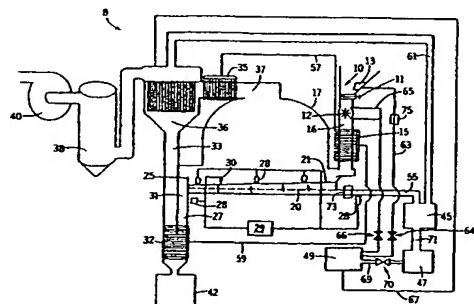
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(57) Abstract: A method and apparatus for the application of heat to remove ammonia compounds from fly ash, thereby making the fly ash a marketable product is disclosed. The method includes the steps of providing an amount of fly ash wherein at least a portion of the amount of fly ash comprises particulates having ammonia compounds affixed to the particulates, and exposing the fly ash to flowing air having a temperature of at least 1,500 °F (815 °C) such that the fly ash is maintained in the flowing air until the fly ash reaches a temperature of at least 900 °F (482 °C). The apparatus (8, 9) includes a source of fly ash (10) comprising particulates having ammonia compounds affixed to at least some of the fly ash particulates, a heating chamber (17) including a treatment bed comprising a floor (20) having openings, a fly ash supply conduit (16) in communication with the heating chamber (17) and the source of fly ash (10) for transferring fly ash from the source of fly ash to the treatment bed of the heating chamber, a source of heated air (45), an air supply conduit (55) in communication with the source of heated of heated air (45) and the heating chamber (17) for providing a flow of heated air to the treatment bed of the heating chamber for contacting the fly ash on the treatment bed with the flow of heated air, a heated air conduit (27) in communication with the heating chamber (17) for transferring the flow of heated air form the heating chamber, and an ash removal conduit (31) in communication with the heating chamber (17) for transferring heated fly ash from the heating chamber.

AMMONIA REMOVAL FROM FLY ASH

CROSS-REFERENCE TO RELATED APPLICATION

This application claims priority from United States Provisional Patent Application No. 60/149,295 filed August 17, 1999.

BACKGROUND OF THE INVENTION

5 This invention relates to the treatment of coal ash to remove ammonia compounds that contaminate the ash as part of post-combustion treatments of exhaust gases to remove nitrogen compounds.

In 1990, the United States Environmental Protection Agency put into place
the Clean Air Act Amendments which were designed to reduce the emissions of
10 "greenhouse gases". Among the emissions covered are the nitrogen compounds
NO and NO₂ referred to generically as NOx. NOx is generated through the
combustion of coal and its generation is directly affected by combustion
temperature, residency time and available oxygen. Several technologies have
been developed to meet the mandated NOx reduction limits.

15 The NOx reduction technologies fall into two major categories. One category includes technologies that modify or control the combustion or firing characteristics. The effect of these approaches has been an increase in residual unburned carbon in the coal ash. The other category includes technologies that are employed after combustion has taken place. These technologies include
20 selective non-catalytic reduction, selective catalytic reduction, and amine enhanced fuel lean gas reburn. These technologies involve adding ammonia (NH₃), and a significant amount of the ammonia finds its way onto the coal ash, typically by combining with available sulphur and other compounds that attach to the ash particles.

25 Coal ash is a marketable product if it is not contaminated. The ash may be used, for example, in concrete products as a replacement for a portion of the cement. However, ash that has been treated to reduce NOx and which is contaminated either by unburned carbon or ammonia compounds is not

marketable.

Systems have been developed which may be used to reduce the amount of ammonia compounds affixed to fly ash. For example, German Patent Application No. 3526756 describes a process for the reduction of ammonia residues from the treated fly ash of a steam generator. In this process, ammonia contaminated fly ash is treated with a hot treating gas, e.g., air heated to 700°C to 800°C, so that the ammonia is driven off into the treating gas. In U.S. Patent No. 4,911,900, there is disclosed an apparatus in which fly ash containing ammonium salts is recovered from the flue gas of a combustion chamber and then introduced into a fluidized bed apparatus in which ammonia is driven off from the fly ash. The stripping of ammonia from the fly ash is affected in the fluidized bed apparatus by direct heating with a hot gas at 700°C to 800°C. Ammonia containing gas from the fluidized bed apparatus is then supplied to an ammonia scrubber from which an ammonia solution is removed for storage. While these systems may be suitable for certain installations, they do have efficiency problems, such as excessive heat loss, that may limit their use in cost sensitive installations.

Therefore, there is a need for an improved method and apparatus that can solve the unburned carbon and ammonia contamination problems in fly ash. More particularly, there is a need for an improved method and apparatus that can remove ammonia compounds from fly ash, and/or consume unburned carbon in fly ash to make the fly ash a marketable product.

SUMMARY OF THE INVENTION

Accordingly, the present invention is directed to a method and apparatus for the application of heat to remove ammonia compounds from fly ash, thereby making the fly ash a marketable product. The method of the invention is directed to a method for reducing the amount of ammonia compounds affixed to fly ash including the steps of providing an amount of fly ash wherein at least a portion of the amount of fly ash comprises particulates having ammonia compounds affixed to the particulates, and exposing the fly ash to flowing air having a temperature of at least 1,500°F (815°C) such that the fly ash is maintained in the flowing air until

the fly ash reaches a temperature of at least 900°F (482°C).

The apparatus of the invention is directed to an apparatus for reducing the amount of ammonia compounds affixed to fly ash wherein the apparatus includes a source of fly ash comprising particulates having ammonia compounds affixed to 5 at least some of the fly ash particulates, a heating chamber including a treatment bed comprising a media having openings, a fly ash supply conduit in communication with the heating chamber and the source of fly ash for transferring fly ash from the source of fly ash to the treatment bed of the heating chamber, a source of heated air, an air supply conduit in communication with the source of 10 heated air and the heating chamber for providing a flow of heated air to the treatment bed of the heating chamber for contacting the fly ash on the treatment bed with the flow of heated air, a heated air conduit in communication with the heating chamber for transferring the flow of heated air from the heating chamber, and an ash removal conduit in communication with the heating chamber for 15 transferring heated fly ash from the heating chamber.

Fly ash is a particulate material collected from the effluent, or flue gases, of stationary combustion sources, such as coal, oil, or municipal solid waste burning power plants. It generally comprises a very fine dust with particles mostly in the silt size range. The physical and chemical properties of fly ash vary according to 20 the combustion source, depending on the source of fuel, burning and handling methods, and also the addition of materials both prior to and subsequent to combustion (such as nitrogenous NO_x reducing treatment agents), as well as the addition of materials to aid in the fly ash collection process.

The principle constituents of fly ash are silica (silicon dioxide, SiO₂), 25 alumina (aluminum oxide, Al₂O₃), calcium oxide (CaO), and iron oxide (FeO). As is well known, the actual composition of fly ash can vary widely, and in fact, the ranges provided are merely representative of common fly ash compositions. In addition to those compositions detailed above, common combustion fly ashes 30 also contain other components, as well as unburned carbon. Generally, fly ashes have a specific gravity which can range between about 2.1 and about 2.6. Most of the particles of fly ash are glassy spheres, except for the carbon particles,

which are somewhat larger and more angular than the inorganic particles. Fly ash particles generally have an average size which can range from less than about 1.0 to about 80 microns in diameter, more commonly between about 1.0 and about 30.0 microns in diameter.

5 The fly ash is generated by the combustion of coal, oil, municipal solid waste, or other materials in a stationary combustion source such as an electricity generating utility or other like system. The fly ash is carried along with the combustion effluent, which often contains nitrogen oxides, a known pollutant. Nitrogen oxides are created when atomic oxygen and nitrogen are formed in the
10 high temperature atmosphere generated.

The nitrogen oxides level in the combustion effluent can be reduced by the introduction of a nitrogenous treatment agent, either in and of itself or to facilitate a selective catalytic reduction process. The most common agents for the non-catalytic reduction of nitrogen oxides are urea and ammonia, which can be
15 introduced according to a number of different processes effective for reducing nitrogen oxides. The catalytic reduction of nitrogen oxides generally involves passing the effluent across the catalyst bed in the presence of ammonia. Selective catalytic reduction processes for reducing NOx are well known and utilize a variety of catalytic agents.

20 Regardless of the specific method by which nitrogen oxides are being reduced by the introduction of a nitrogenous treatment agent, it is virtually impossible to prevent at least some ammonia from affixing to fly ash. When this occurs, ammonia becomes affixed to the fly ash, primarily by being reacted therewith, and is absorbed onto the fly ash. Most often, the ammonia is present
25 on the ash in the form of ammonium salts, such as ammonium chloride, ammonium sulfate, and ammonium bisulfate, as well as absorbed free ammonia. As used herein, the term "ammonia compounds" shall be used to refer to these substances, that is, ammonia (NH_3) and compounds including the ammonium ion (NH_4^+).

30 In order to prevent the fly ash from being emitted to the atmosphere, it is collected by conventional apparatus such as in a baghouse, an electrostatic

precipitator, or like means. The ash is then transported either to disposal, such as in a landfill or strip mine, or to be reused such as for structural fill or in the formation of cement or other building materials.

In order to liberate or strip the affixed ammonia from the combustion fly ash after it has been collected as described above, it is exposed to moving air under conditions effective to strip a substantial amount of the ammonia from the ash. Although this description is written in terms of moving air, the term will be understood to include dry air, as well as air containing water vapor, and steam.

It is therefore an advantage of the present invention to provide an effective and efficient system and apparatus for removing ammonia compounds and other contaminants from fly ash.

BRIEF DESCRIPTION OF THE DRAWINGS

The features, aspects, and advantages of the present invention will become better understood upon consideration of the following detailed description, appended claims and accompanying drawings where:

Figure 1 is a diagrammatic illustration of an apparatus for carrying out the invention; and .

Figure 2 is a diagrammatic illustration of another embodiment of an apparatus for carrying out the invention.

It should be understood that the drawings are not necessarily to scale and that the embodiments are sometimes illustrated by phantom lines, diagrammatic representations and fragmentary views. In certain instances, details which are not necessary for an understanding of the present invention or which render other details difficult to perceive may have been omitted. It should be understood, of course, that the invention is not necessarily limited to the particular embodiments illustrated herein.

Like reference numerals will be used to refer to like or similar parts from Figure to Figure in the following description of the drawings.

DETAILED DESCRIPTION OF THE INVENTION

Referring to Figure 1, there is shown an apparatus, indicated generally at 8, for reducing the amount of ammonia compounds affixed to fly ash. The

apparatus 8 includes an ash storage unit 10 that holds the ammonia contaminated ash that will be treated in the process of the invention. The ash may be coal ash from coal boilers utilizing NOx reduction systems incorporating ammonia compounds. Typically, such systems collect ashes through a dry process such as an electrostatic precipitator, a baghouse or a cyclone. The ash storage unit 10 may be a standard storage silo, preferably configured with sufficient height to allow for gravity feed. A maintenance gate 11 closes the bottom of the ash storage unit 10 to halt the flow of ash for maintenance of the equipment downstream. The ash storage unit 10 may be replaced by a feed directly from equipment that is collecting the ash from a furnace and NOx removal system. Ashes collected from the NOx removal system of a furnace typically maintain a temperature of 110°F (43°C) or higher. Preferably, process equipment is selected to maintain or increase this temperature. For example, the ash storage unit 10 may have insulated walls or may include aeration stones 13 which receive air from an air supply unit 49 via conduit 63 (having pressure gauge 75) for aeration of the ash with heated air.

The ammonia contaminated ash is fed from the ash storage unit 10 through a rotary air lock in the form of a high temperature rotary feeder 12. The rotary feeder 12 receives air from the air supply unit 49 via conduit 65 with an inline valve 66 that assists in maintaining a steady feed and depth of ash to a preheating section which includes an ash preheater 15. A suitable rotary feeder is available from Delta/Ducon Conveying Technology, Inc., Malvern, Pennsylvania, USA. The ash flows through conduit 16 wherein ash preheater 15 preheats the ash preferably to 300°F (148°C) or above, and most preferably to approximately 500°F (260°C), using a bulk flow heat exchanger in the form of a series of vertical plates. The plates of the ash preheater 15 receive heat from a bulk flow heat exchanger 32 via conduit 59 and from a heat recovery unit 35 via conduit 57 as will be described further below. A suitable ash preheater is available from Cominco Engineering Services of Calgary, Alberta, Canada.

The preheated ash is fed into an insulated heating chamber 17 either as a batch or continuous process. The chamber 17 includes a treatment bed with a

downwardly sloping floor 20 formed of a porous metal material, preferably an alloy sold under the designation "Inconel 600". Either a vibratory feeder or a rotary vane feeder may be used to deposit the preheated ash onto the floor 20. A vibratory feeder is preferred due to its economy of operation and high heat applicability. Hot air is passed through the porous metal material of the floor 20 to provide both heat and fluidization to move the ash deposited on the floor 20. The result is a fluidized bed conveyor 21. A suitable fluidized bed conveyor is available as an airstide from Delta/Ducon Conveying Technology, Inc., Malvern, Pennsylvania, USA. The porous metal media that supports the ash bed may be 0.062 inches (1.57 millimeters) thick and preferably has openings of 10 microns or less. A suitable porous metal media is available from Mott Metallurgical Corporation of Farmington, Connecticut, USA.

The heated air is passed through the porous metal media of the floor 20 to provide for uniform aeration and heating of the ash bed. The hot aeration air is provided such that a minimum of ash particles are carried out of the treatment area. This is accomplished through the design of the porous media sizing, the aeration air pressure and the air temperature. The heated air is passed through the ash bed at a specific flow rate which is designed to maximize the heat uptake by the ash bed and provide for the removal of the decomposed ammonia compounds. The same aeration air provides the fluidization to move the ash through the heating chamber in a continuous process or to move ash out of the chamber in a batch system.

The hot air passed through the floor 20 may come from a direct fired natural gas burner, oil fired burner, electrical heat source, or waste heat source, such as the waste heat of a combustion turbine. In the apparatus of Figure 1, the hot air passed through the floor 20 comes via a conduit 55 from a gas furnace 45 that receives preheated air from an air preheater 47 via a conduit 71. The air preheater 47 receives air from the air supply unit 49 (such as a compressor) via a conduit 69 with an inline valve 70 that controls the flow of air into the air preheater 47. A programmable logic controller 29 receives signals from a pressure gauge 73 in the conduit 55 and provides control signals to valve 70 in order to control air

flow into the air preheater 47 and the furnace 45. Preferably, the hot air is supplied to the floor 20 from the furnace 45 at a pressure from greater than 0 to about 3 psi (0.0207 MPa). At these pressures, the metal media will pass air heated at a temperature of at least 1500°F (815°C), and preferably in the range of 5 1500°F (815°C) to 1700°F (927°C), into the ash bed 21 at approximately 0 to about 10 cubic feet (0.28 cubic meters) per minute. One advantage to using flowing air having a temperature of at least 1500°F (815°C) is that more rapid heating of the fly ash and a resulting faster release of ammonia compounds occurs. The ammonia compounds common to NO_x reduction technologies are 10 liberated from the ash by heats of at least 900°F (482°C), preferably 980°F (526°C) or greater, and are carried away from the ash by the air. Temperatures in excess of 900°F (482°C) provide increased process efficiencies. For example, one advantage to heating the ash to temperatures of at least 900°F (482°C) is that complete removal of ammonia compounds from the fly ash occurs. Ammonia 15 may be found on fly ash as several different compounds, such as ammonium bisulfate and ammonium sulfate. It has been discovered that the removal temperature for ammonium bisulfate is 813°F (434°C) and the removal temperature for ammonium sulfate is 808°F (431°C), while other ammonia compounds are liberated at lower temperatures. By heating the ash to 20 temperatures of at least 900°F (482°C), it is assured that the various ammonia compounds are removed from the fly ash. The liberating air also provides the motive force or fluidization that allows the ash particles to move within the treatment bed.

The ash should be retained in the treatment bed 21 until it reaches a 25 minimum temperature of 900°F (482°C). A blocking means such as a weir or a dam 25 is used to retain the ash in the heating chamber 17. As ash is fed into the beginning of the bed 21, the fluidized ash level rises. As the ash level rises, the clean ash at the exit area spills over the weir or dam 25 and drops through conduit 31 into a heat recovery zone 27. A series of thermocouples 28 in electric 30 communication with the controller 29 may be used to control the valve 66 that controls air input to the rotary feeder 12 to control ash input to the heating

chamber 17 in response to the measured ash exit temperature. As the target temperature is reached by the ash, more ash is fed into the bed 21 via the rotary feeder 12. The programmable logic controller 29 uses data from the thermocouples 28 and a level probe 30 to monitor and control heat exchange rates, to control ash feed rates from the rotary feeder 12, to control treatment bed air flow from the furnace 45 (by control of valve 70) and to monitor ash temperatures within the system.

An alternative to using a weir or dam 25 as the ash outflow blocking means is the use of a gate to retain ash in the heating chamber 17. As the ash in the heating chamber 17 reaches the designated temperature as determined by thermocouples 28 in electrical communication with controller 29, the controller 29 causes the gate to raise allowing a portion of heated ash to exit the bed 21. The controller 29 also causes ash to be fed into the bed 21 via rotary feeder 12. The use of a gate mechanism aids in preventing incoming ash from short circuiting the bed 21; allowing only heated ash from the bottom of the ash bed and in close contact with the incoming hot air, to exit the heating chamber 17.

The heat recovery zone 27 is equipped with a bulk flow heat exchanger 32 which transfers heat from the treated ash to the plates of the ash preheater 15 via conduit 59 as described above. The ash leaving the system is cooled and transferred to a storage unit 42. Dilute pneumatic transfer from the heat recovery zone 27 to the storage unit 42 may be used to further cool the ash. The ash in storage unit 42 may then be stored and managed using conventional means.

The upper portion of the heating chamber 17 is domed to provide a static pressure area. The gases and any entrained fly ash from the heating chamber 17 pass through conduit 37 into a heat recovery unit 35 in the form of a heat exchanger which transfers heat from the gases and any entrained fly ash to the plates of the ash preheater 15 via conduit 57 as described above. The heat recovery unit 35 cools the gas and entrained fly ash mixture and provides heat to the ash in the pretreatment area via ash preheater 15. The gas and entrained fly ash mixture may then pass to a high temperature baghouse 36 operated at a temperature in excess of 400°F (204°C) to ensure that the ammonia contaminants

remain in a gaseous state thereby inhibiting reformation and deposition of the ammonia compounds on the ash and equipment surfaces. A suitable high temperature baghouse is available from Bundy Environmental Technology, Inc., Reynoldsburg, Ohio, USA. The baghouse 36 captures fugitive ash particles, and
5 the clean ash collected by the baghouse 36 is transferred via conduit 33 to the heat recovery zone 27 where the bulk flow heat exchanger 32 transfers heat from the fly ash to the plates of the ash preheater 15 via conduit 59 as described above. The fly ash leaving the system is cooled and transferred to a storage unit 42. Dilute pneumatic transfer may be used to further cool the fly ash.

10 A contaminated air stream also exits the baghouse 36 and enters a wet scrubber 38 where the ammonia and other contaminants are collected. The scrubbing liquor may be alkaline or acidic, depending on the desires of the facility using the apparatus 8. An acidic media will capture several gas constituents including ammonia and sulfur. An alkaline media will capture the sulfur while
15 allowing the ammonia to pass to the next stage. The scrubber 38 also provides for quenching of the hot gases to a temperature that will not harm a fan 40 that creates a negative pressure on the system to carry contaminated air from the bed 21 through the baghouse 36 and through the wet scrubber 38. Preferably, the induced draft fan 40 pulls a negative pressure on the heating chamber 17 of
20 approximately 1 - 3 inches (25.4 - 76.2 millimeters) of water to provide the motive force to draw gas through the baghouse 36 and the scrubber 38. The type of scrubbing system employed determines whether the collected contaminants are disposed of or processed for utilization. The scrubber system may be that supplied by Bionomic Industries of Oceanside, California, USA.

25 Turning now to Figure 2, there is shown an another embodiment of an apparatus, indicated generally at 9, for the removal of ammonia compounds from fly ash. The apparatus 9 has many of the components and operating parameters as the apparatus 8 shown in Figure 1. However, in the apparatus 9 of Figure 2, the baghouse 36, the wet scrubber 38 and the fan 40 are removed from the
30 apparatus 8 as shown in Figure 1. In the apparatus 9 of Figure 2, the gases and any entrained fly ash from the heating chamber 17 are cooled below 400°F

(204°C) and directed towards the inlet duct of a NOx treatment system 81 (such as a selective catalytic reduction system) that receives exhaust gases from a steam generator 78 (such as a coal combustion boiler) via conduit 79. The NOx treatment system 81 utilizes the ammonia that was liberated from the ash in the heating chamber 17. A portion of the gases and any entrained fly ash from the heating chamber 17 may also be introduced into the steam generator 78 via conduit 83 having inline valve 84.

The use of the present invention to achieve substantial reductions in the amount of ammonia compounds affixed to post-combustion fly ash and to achieve reductions in loss on ignition (carbon) levels is illustrated by the following 10 laboratory tests that were performed on fly ash conforming to specifications of the American Society for Testing and Materials (ASTM) for fly ash used in concrete.

Example 1

A sample of ASTM C-618 Class C fly ash containing ammonia was obtained from a coal fired steam generator. The sample of fly ash was measured for ammonia levels and it was determined that the ammonia levels were 51 mg./kg. The sample of fly ash was also measured for loss on ignition (carbon) levels and it was determined that the loss on ignition (carbon) levels were 0.4%. The sample of fly ash was then continuously heated at 1000°F (538°C) until a constant mass was attained and thus no loss on ignition (carbon) remained in the fly ash. The heated sample of fly ash was then measured for ammonia levels and it was determined that the ammonia levels were less than 2 mg./kg. This test confirmed that both ammonia and loss on ignition (carbon) were removed from the sample of ASTM C-618 Class C fly ash containing ammonia when heated at 20 1000°F (538°C).
25

Example 2

A sample of ASTM C-618 Class F fly ash containing ammonia was obtained from another coal fired steam generator. The sample of fly ash was measured for ammonia levels and it was determined that the ammonia levels 30 were 170 mg./kg. The sample of fly ash was also measured for loss on ignition (carbon) levels and it was determined that the loss on ignition (carbon) levels

were 2.9%. The sample of fly ash was then continuously heated at 1000°F (538°C) until a constant mass was attained and thus no loss on ignition (carbon) remained in the fly ash. The heated sample of fly ash was then measured for ammonia levels and it was determined that the ammonia levels were less than 2 mg./kg. This test confirmed that both ammonia and loss on ignition (carbon) were removed from the sample of ASTM C-618 Class F fly ash containing ammonia when heated at 1000°F (538°C).

Although the present invention has been described in considerable detail
10 with reference to certain embodiments, one skilled in the art will appreciate that
the present invention can be practiced by other than the described embodiments,
which have been presented for purposes of illustration and not of limitation.
Therefore, the scope of the appended claims should not be limited to the
description of the embodiments contained herein.

CLAIMS

1. A method for reducing the amount of ammonia compounds affixed to fly ash, the method comprising:

providing an amount of fly ash, at least a portion of the amount of fly ash comprising particulates having ammonia compounds affixed to the particulates; and

exposing the amount of fly ash to flowing air having a temperature of at least 1,500°F (815°C).

2. The method of claim 1 wherein:

the fly ash is maintained in the flowing air until the fly ash reaches a temperature of at least 900°F (482°C).

3. The method of claim 1 further comprising:

measuring an in process ash temperature of the fly ash when the fly ash is exposed to the flowing air;

removing at least a portion of the fly ash being exposed to the flowing air when the measured in process ash temperature reaches at least 900°F (482°C);

thereafter providing a second amount of fly ash, at least a portion of the second amount of fly ash comprising particulates having ammonia compounds affixed to the particulates; and

thereafter exposing the second amount of fly ash to flowing air having a temperature of at least 1,500°F (815°C).

4. The method of claim 1 further comprising:

preheating the fly ash to a temperature of at least 300°F (148°C) before exposing the fly ash to the flowing air.

5. The method of claim 1 further comprising:

recovering heat from the flowing air after the fly ash has been exposed to

the flowing air.

6. The method of claim 5 further comprising:
using the heat recovered from the flowing air to preheat a second amount
of fly ash, at least a portion of the second amount of fly ash comprising
particulates having ammonia compounds affixed to the particulates; and
thereafter exposing the second amount of fly ash to flowing air having a
temperature of at least 1,500°F (815°C).

7. The method of claim 6 wherein:
the second amount of fly ash is preheated to a temperature of at least
300°F (148°C)

8. The method of claim 5 further comprising:
removing particulate material from the flowing air after heat has been
recovered from the flowing air.

9. The method of claim 8 further comprising:
maintaining the flowing air above 400°F (204°C) when particulate material
is removed from the flowing air.

10. The method of claim 8 further comprising:
recovering heat from the particulate material after the particulate material
has been removed from the flowing air.

11. The method of claim 10 further comprising:
using the heat recovered from the particulate material to preheat a second
amount of fly ash, at least a portion of the second amount of fly ash comprising
particulates having ammonia compounds affixed to the particulates; and
thereafter exposing the second amount of fly ash to flowing air having a
temperature of at least 1,500°F (815°C).

12. The method of claim 11 wherein:
the second amount of fly ash is preheated to a temperature of at least
300°F (148°C)
13. The method of claim 1 further comprising:
recovering heat from the fly ash after the fly ash has been exposed to the
flowing air.
14. The method of claim 13 further comprising:
using the heat recovered from the fly ash to preheat a second amount of fly
ash, at least a portion of the second amount of fly ash comprising particulates
having ammonia compounds affixed to the particulates; and
thereafter exposing the second amount of fly ash to flowing air having a
temperature of at least 1,500°F (815°C).
15. The method of claim 14 wherein:
the second amount of fly ash is preheated to a temperature of at least
300°F (148°C)
16. The method of claim 1 wherein the step of exposing the fly ash to
flowing air comprises:
providing a metal media having openings;
passing flowing air through the openings; and
depositing the fly ash on the metal media.
17. The method of claim 16 wherein:
the openings are 10 microns or less.
18. The method of claim 16 wherein:
the flowing air is passed through the openings at greater than 0 to about
10 cubic feet (0.28 cubic meters) per minute.

19. The method of claim 1 further comprising:
 - measuring an in process ash temperature of the fly ash when the fly ash is exposed to the flowing air; and
 - controlling a flow rate of the flowing air in response to the measured in process ash temperature.
20. A method for reducing the amount of ammonia compounds affixed to fly ash, the method comprising:
 - providing an amount of fly ash, at least a portion of the amount of fly ash comprising particulates having ammonia compounds affixed to the particulates; and
 - exposing the amount of fly ash to flowing air until the fly ash reaches a temperature of at least 900°F (482°C).

21. An apparatus for reducing the amount of ammonia compounds affixed to fly ash, the apparatus comprising:
 - a source (10) of fly ash, at least a portion of the fly ash comprising particulates having ammonia compounds affixed to the particulates;
 - a heating chamber (17) including a treatment bed (20) comprising a media having openings;
 - a fly ash supply conduit (16) in communication with the heating chamber (17) and the source (10) of fly ash, the fly ash supply conduit (16) transferring fly ash from the source (10) of fly ash to the treatment bed (20) of the heating chamber (17);
 - a source (45) of heated air;
 - an air supply conduit (55) in communication with the source (45) of heated air and the heating chamber (17), the air supply conduit (55) providing a flow of heated air to the treatment bed (20) of the heating chamber (17) for contacting the fly ash on the treatment bed (20) with the flow of heated air;
 - a heated air conduit (37) in communication with the heating chamber (17) for transferring the flow of heated air from the heating chamber (17); and
 - an ash removal conduit (31) in communication with the heating chamber (17) for transferring heated fly ash from the heating chamber (17).
22. The apparatus of claim 21 further comprising:
 - a heater (15) for heating the fly ash passing through the fly ash supply conduit (16).
23. The apparatus of claim 21 further comprising:
 - a heat recovery unit (32) for recovering heat from heated fly ash passing through the ash removal conduit (31).
24. The apparatus of claim 23 further comprising:
 - a heater (15) for heating the fly ash passing through the fly ash supply conduit (16), the heater (15) receiving heat recovered by the heat recovery unit

(32) from heated fly ash.

25. The apparatus of claim 21 further comprising:
a heat recovery unit (35) for recovering heat from the flow of heated air passing through the heated air conduit (37).
26. The apparatus of claim 25 further comprising:
a heater (15) for heating the fly ash passing through the fly ash supply conduit (16), the heater (15) receiving heat recovered by the heat recovery unit (35) from the flow of heated air.
27. The apparatus of claim 25 further comprising:
a particulate filter (36) in communication with the heated air conduit (37), the particulate filter (36) removing particulate material from the flow of heated air from the heating chamber (17).
28. The apparatus of claim 27 further comprising:
a particulate material conduit (33) for transferring particulate material from the particulate filter (36),
wherein a second heat recovery unit (32) recovers heat from the particulate material passing through the particulate material conduit (33).
29. The apparatus of claim 25 further comprising:
a nitrogen oxide treatment system (81) in communication with the heated air conduit (37) for receiving the flow of heated air from the heating chamber (17).
30. The apparatus of claim 21 wherein:
the media is made from a metallic material and has openings of 10 microns or less.

31. The apparatus of claim 21 further comprising:
 - a controller (29) in electrical communication with at least one temperature sensor (28) for sensing a temperature of the fly ash on the treatment bed (20); and
 - a feeder (12) for controlling the feed of fly ash from the source (10) of fly ash to the fly ash supply conduit (16), the feeder controlling the feed of fly ash in dependence on the sensed temperature of the fly ash on the treatment bed (20).
32. The apparatus of claim 21 further comprising:
 - a controller (29) in electrical communication with at least one temperature sensor (28) for sensing a temperature of the fly ash on the treatment bed (20); and
 - a valve (70) for controlling the flow rate of heated air to the treatment bed (20) of the heating chamber (17) from the source (45) of heated air in dependence on the sensed temperature of the fly ash on the treatment bed (20).
33. The apparatus of claim 21 further comprising:
 - aeration stones (13) in the source (10) of fly ash, the aeration stones (13) receiving air from an air supply unit (49) for aeration of the fly ash.
34. The apparatus of claim 21 wherein:
 - the treatment bed (20) of the heating chamber (17) is downwardly sloped.
35. The apparatus of claim 34 wherein:
 - a lower section of the treatment bed (20) includes a blocking means (25) to control flow of heated fly ash from the heating chamber (17).

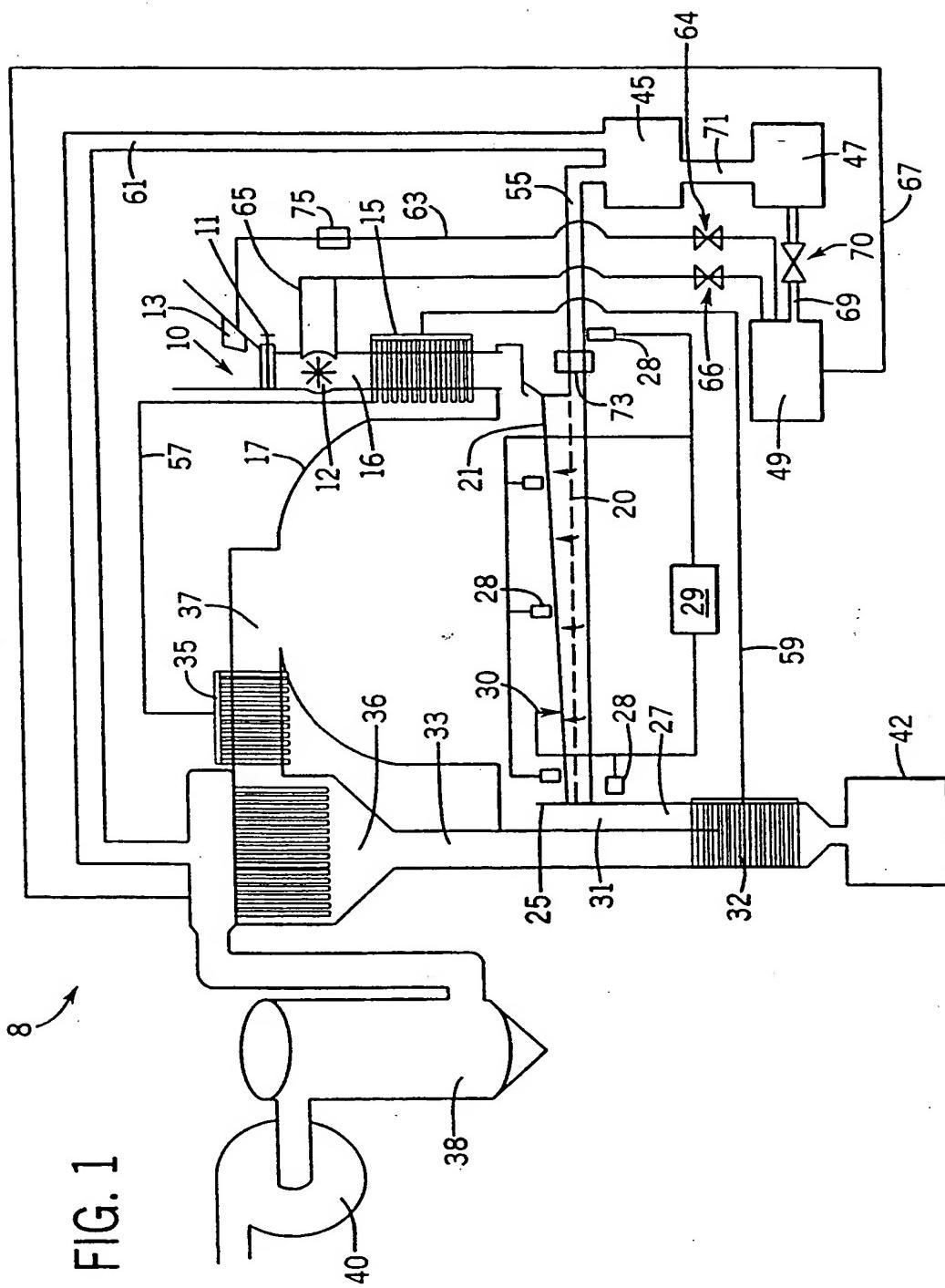


FIG. 1

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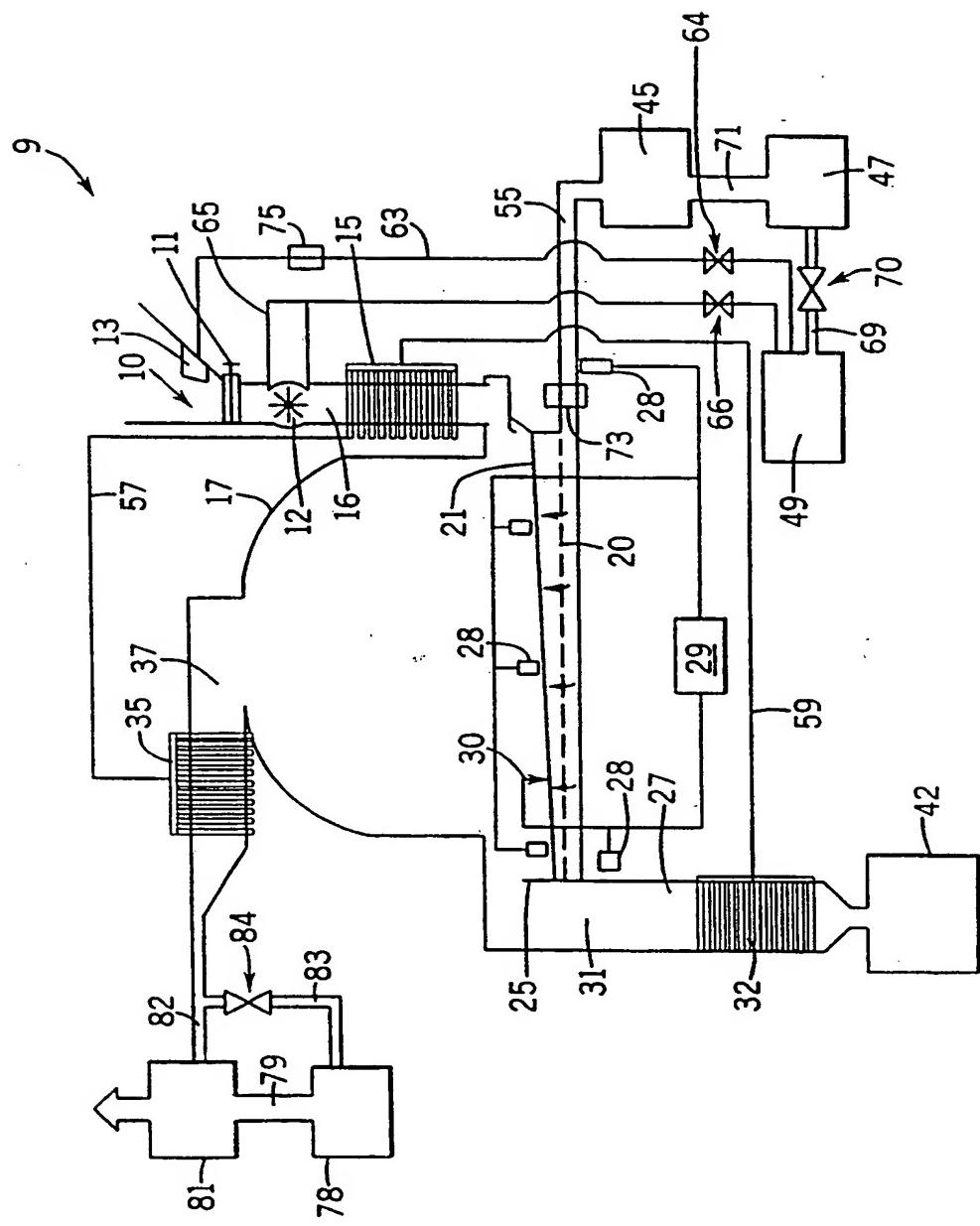


FIG. 2

INTERNATIONAL SEARCH REPORT

International Application No
PCT/US 00/22398

A. CLASSIFICATION OF SUBJECT MATTER				
IPC 7	A62D3/00	C01C1/02	B09B3/00	C22B7/02
				B01D53/56

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)
IPC 7 A62D C01C B09B C22B B01D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

WPI Data, PAJ, EPO-Internal

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	DE 38 02 884 A (PETERS AG CLAUDIUS) 10 August 1989 (1989-08-10) the whole document ----	1-3, 5, 13, 16, 19-21, 23, 25, 29, 31-33
X	PATENT ABSTRACTS OF JAPAN vol. 004, no. 089 (C-016), 25 June 1980 (1980-06-25) & JP 55 054075 A (MITSUBISHI HEAVY IND LTD), 21 April 1980 (1980-04-21) abstract ----	1, 20, 21
X	DE 34 25 070 A (STEAG AG) 16 January 1986 (1986-01-16) page 5, line 17 - line 23; claims; figure 1 ----	20, 21, 23
		-/-

Further documents are listed in the continuation of box C.

Patent family members are listed in annex.

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Date of the actual completion of the international search

4 December 2000

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Eijkenboom, A

INTERNATIONAL SEARCH REPORT

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C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
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X	US 4 911 900 A (HORCH KLAUS ET AL) 27 March 1990 (1990-03-27) cited in the application column 4, line 29 - line 35; figures 1,2 ----	20
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X	DE 37 08 941 A (STEAG AG) 29 September 1988 (1988-09-29) column 3, line 28 -column 4, line 1; figures ----	20
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